

Chemical Engineering Thermodynamics
Quiz 1 January 14, 2016

1)

P1.1. Estimate the average speed (mph) of hydrogen molecules at 200 K and 3 bars.

H₂ is 2.02 g/mole

R = 8.314 J/(K mole)

Joule = kg m²/s²

2.24 mph/(m/s)

You can assume you know the temperature and pressure to 10% accuracy or you can make some other assumption concerning the accuracy of these values (state your assumption).

2)

1.12. The gas phase reaction $A \rightarrow 2R$ is conducted in a 0.1 m³ spherical tank. The initial temperature and pressure in the tank are 0.05 MPa and 400 K. After species A is 50% reacted, the temperature has fallen to 350 K. What is the pressure in the vessel?

R = 8.314 cm³ MPa/(K mole)

3)

1.17. Determine the temperature, volume, and quality for one kg water under the following conditions:

a. $U = 3000$ kJ/kg, $P = 0.3$ MPa

c. $U = 2500$ kJ/kg, $P = 0.3$ MPa

See tables below.

E.9. Properties of Water¹

I. Saturation Temperature

T (°C)	P (MPa)	v^L m ³ /kg	v^V m ³ /kg	u^L kJ/kg	Δu^{vap} kJ/kg	u^V kJ/kg	h^L kJ/kg	Δh^{vap} kJ/kg	h^V kJ/kg	s^L kJ/kg-K	Δs^{vap} kJ/kg-K	s^V kJ/kg-K
0.01	0.000612	0.001000	205.9912	0.00	2374.92	2374.92	0.00	2500.92	2500.92	0.0000	9.1555	9.1555
5	0.000873	0.001000	147.0113	21.02	2360.76	2381.78	21.02	2489.04	2510.06	0.0763	8.9485	9.0248
10	0.001228	0.001000	106.3032	42.02	2346.63	2388.65	42.02	2477.19	2519.21	0.1511	8.7487	8.8998
15	0.001706	0.001001	77.8755	62.98	2332.51	2395.49	62.98	2465.35	2528.33	0.2245	8.5558	8.7803
20	0.002339	0.001002	57.7567	83.91	2318.41	2402.32	83.91	2453.52	2537.43	0.2965	8.3695	8.6660
25	0.003170	0.001003	43.3373	104.83	2304.30	2409.13	104.83	2441.68	2546.51	0.3672	8.1894	8.5566
30	0.004247	0.001004	32.8783	125.73	2290.18	2415.91	125.73	2429.82	2555.55	0.4368	8.0152	8.4520
35	0.005629	0.001006	25.2053	146.63	2276.04	2422.67	146.63	2417.92	2564.55	0.5051	7.8466	8.3517
40	0.007385	0.001008	19.5151	167.53	2261.86	2429.39	167.53	2405.98	2573.51	0.5724	7.6831	8.2555
45	0.009595	0.001010	15.2521	188.43	2247.65	2436.08	188.43	2394.00	2582.43	0.6386	7.5247	8.1633
50	0.012400	0.001012	12.0269	209.33	2233.40	2442.73	209.34	2381.95	2591.29	0.7038	7.3710	8.0748
55	0.015800	0.001015	9.5643	230.24	2219.10	2449.34	230.26	2369.83	2600.09	0.7680	7.2218	7.9898
60	0.019900	0.001017	7.6672	251.16	2204.74	2455.90	251.18	2357.65	2608.83	0.8313	7.0768	7.9081
65	0.025000	0.001020	6.1935	272.09	2190.32	2462.41	272.12	2345.38	2617.50	0.8937	6.9359	7.8296
70	0.031200	0.001023	5.0395	293.03	2175.83	2468.86	293.07	2333.03	2626.10	0.9551	6.7989	7.7540
75	0.038600	0.001026	4.1289	313.99	2161.25	2475.24	314.03	2320.57	2634.60	1.0158	6.6654	7.6812
80	0.047400	0.001029	3.4052	334.96	2146.60	2481.56	335.01	2308.01	2643.02	1.0756	6.5355	7.6111
85	0.057900	0.001032	2.8258	355.95	2131.86	2487.81	356.01	2295.32	2651.33	1.1346	6.4088	7.5434
90	0.070200	0.001036	2.3591	376.97	2117.00	2493.97	377.04	2282.49	2659.53	1.1929	6.2852	7.4781
95	0.084600	0.001040	1.9806	398.00	2102.04	2500.04	398.09	2269.52	2667.61	1.2504	6.1647	7.4151
100	0.101400	0.001043	1.6718	419.06	2086.96	2506.02	419.17	2256.40	2675.57	1.3072	6.0469	7.3541
105	0.120900	0.001047	1.4184	440.15	2071.75	2511.90	440.27	2243.12	2683.39	1.3633	5.9319	7.2952
110	0.143400	0.001052	1.2093	461.26	2056.41	2517.67	461.42	2229.64	2691.06	1.4188	5.8193	7.2381
115	0.169200	0.001056	1.0358	482.41	2040.92	2523.33	482.59	2215.99	2698.58	1.4737	5.7091	7.1828
120	0.198700	0.001060	0.8912	503.60	2025.26	2528.86	503.81	2202.12	2705.93	1.5279	5.6012	7.1291
125	0.232200	0.001065	0.7700	524.83	2009.44	2534.27	525.07	2188.03	2713.10	1.5816	5.4954	7.0770
130	0.270300	0.001070	0.6680	546.09	1993.44	2539.53	546.38	2173.70	2720.08	1.6346	5.3918	7.0264
135	0.313200	0.001075	0.5817	567.41	1977.24	2544.65	567.74	2159.13	2726.87	1.6872	5.2900	6.9772
140	0.361500	0.001080	0.5085	588.77	1960.85	2549.62	589.16	2144.28	2733.44	1.7392	5.1901	6.9293
145	0.415700	0.001085	0.4460	610.19	1944.23	2554.42	610.64	2129.16	2739.80	1.7907	5.0919	6.8826
150	0.476200	0.001091	0.3925	631.66	1927.39	2559.05	632.18	2113.75	2745.93	1.8418	4.9953	6.8371
155	0.543500	0.001096	0.3465	653.19	1910.32	2563.51	653.79	2098.02	2751.81	1.8924	4.9002	6.7926
160	0.618200	0.001102	0.3068	674.79	1892.99	2567.78	675.47	2081.97	2757.44	1.9426	4.8065	6.7491
165	0.700900	0.001108	0.2724	696.46	1875.39	2571.85	697.24	2065.57	2762.81	1.9923	4.7143	6.7066
170	0.792200	0.001114	0.2426	718.20	1857.53	2575.73	719.08	2048.82	2767.90	2.0417	4.6233	6.6650
175	0.892600	0.001121	0.2166	740.02	1839.37	2579.39	741.02	2031.69	2772.71	2.0906	4.5335	6.6241
180	1.002800	0.001127	0.1938	761.92	1820.91	2582.83	763.05	2014.16	2777.21	2.1392	4.4448	6.5840
185	1.123500	0.001134	0.1739	783.91	1802.13	2586.04	785.19	1996.22	2781.41	2.1875	4.3572	6.5447
190	1.255200	0.001141	0.1564	806.00	1783.01	2589.01	807.43	1977.85	2785.28	2.2355	4.2704	6.5059
195	1.398800	0.001149	0.1409	828.18	1763.56	2591.74	829.79	1959.03	2788.82	2.2832	4.1846	6.4678
200	1.554900	0.001157	0.1272	850.47	1743.73	2594.20	852.27	1939.74	2792.01	2.3305	4.0997	6.4302

III. Superheated Steam

$P = 0.01\text{MPa}$ (45.8)					$P = 0.05\text{MPa}$ (81.3)					$P = 0.10\text{MPa}$ (99.6)				
$T(^{\circ}\text{C})$	$V(\text{m}^3/\text{kg})$	$U(\text{kJ}/\text{kg})$	$H(\text{kJ}/\text{kg})$	$S(\text{kJ}/\text{kg}\cdot\text{K})$	$T(^{\circ}\text{C})$	$V(\text{m}^3/\text{kg})$	$U(\text{kJ}/\text{kg})$	$H(\text{kJ}/\text{kg})$	$S(\text{kJ}/\text{kg}\cdot\text{K})$	$T(^{\circ}\text{C})$	$V(\text{m}^3/\text{kg})$	$U(\text{kJ}/\text{kg})$	$H(\text{kJ}/\text{kg})$	$S(\text{kJ}/\text{kg}\cdot\text{K})$
45.8	14.6701	2437.2	2583.9	8.1488	81.3	3.2400	2483.2	2645.2	7.5930	99.6	1.6939	2505.6	2675.0	7.3588
50	14.9139	2443.3	2592.4	8.1755	100	3.4187	2511.5	2682.4	7.6953	100	1.6959	2506.2	2675.8	7.3610
100	17.1964	2515.5	2687.5	8.4489	150	3.8897	2585.7	2780.2	7.9413	150	1.9367	2582.9	2776.6	7.6148
150	19.5132	2587.9	2783.0	8.6892	200	4.3562	2660.0	2877.8	8.1592	200	2.1724	2658.2	2875.5	7.8356
200	21.8256	2661.3	2879.6	8.9049	250	4.8206	2735.1	2976.1	8.3568	250	2.4062	2733.9	2974.5	8.0346
250	24.1361	2736.1	2977.4	9.1015	300	5.2840	2811.6	3075.8	8.5386	300	2.6388	2810.6	3074.5	8.2172
300	26.4456	2812.3	3076.7	9.2827	350	5.7469	2889.4	3176.8	8.7076	350	2.8710	2888.7	3175.8	8.3866
350	28.7545	2890.0	3177.5	9.4513	400	6.2094	2968.9	3279.3	8.8659	400	3.1027	2968.3	3278.6	8.5452
400	31.0631	2969.3	3279.9	9.6094	450	6.6717	3049.9	3383.5	9.0151	450	3.3342	3049.4	3382.8	8.6946
450	33.3714	3050.3	3384.0	9.7584	500	7.1338	3132.6	3489.3	9.1566	500	3.5655	3132.2	3488.7	8.8361
500	35.6796	3132.9	3489.7	9.8998	550	7.5957	3217.0	3596.8	9.2913	550	3.7968	3216.6	3596.3	8.9709
550	37.9876	3217.2	3597.1	10.0344	600	8.0576	3303.1	3706.0	9.4201	600	4.0279	3302.8	3705.6	9.0998
600	40.2956	3303.3	3706.3	10.1631	650	8.5195	3391.0	3816.9	9.5436	650	4.2590	3390.7	3816.6	9.2234
650	42.6035	3391.2	3817.2	10.2866	700	8.9812	3480.6	3929.7	9.6625	700	4.4900	3480.4	3929.4	9.3424
700	44.9113	3480.8	3929.9	10.4055	750	9.4430	3572.0	4044.2	9.7773	750	4.7209	3571.8	4043.9	9.4572
750	47.2191	3572.2	4044.4	10.5202	800	9.9047	3665.2	4160.4	9.8882	800	4.9519	3665.0	4160.2	9.5681
800	49.5269	3665.3	4160.6	10.6311	850	10.3663	3760.1	4278.5	9.9957	850	5.1828	3760.0	4278.2	9.6757
850	51.8347	3760.3	4278.6	10.7386	900	10.8280	3856.8	4398.2	10.1000	900	5.4137	3856.6	4398.0	9.7800
900	54.1424	3856.9	4398.3	10.8429	950	11.2896	3955.1	4519.6	10.2014	950	5.6446	3955.0	4519.5	9.8813
950	56.4501	3955.2	4519.7	10.9442	1000	11.7513	4055.1	4642.7	10.3000	1000	5.8754	4055.0	4642.6	9.9800
1000	58.7578	4055.2	4642.8	11.0428	1050	12.2129	4156.8	4767.4	10.3960	1050	6.1063	4156.6	4767.3	10.0761
1050	61.0655	4156.8	4767.5	11.1389	1100	12.6745	4259.9	4893.7	10.4897	1100	6.3371	4259.8	4893.5	10.1697
1100	63.3732	4260.0	4893.7	11.2325	1150	13.1361	4364.6	5021.4	10.5811	1150	6.5680	4364.5	5021.3	10.2611
1150	65.6808	4364.7	5021.5	11.3239	1200	13.5977	4470.8	5150.7	10.6703	1200	6.7988	4470.7	5150.6	10.3504
1200	67.9885	4470.9	5150.7	11.4132	1250	14.0592	4578.4	5281.3	10.7576	1250	7.0296	4578.3	5281.2	10.4376
1250	70.2961	4578.4	5281.4	11.5004	1300	14.5208	4687.3	5413.3	10.8428	1300	7.2604	4687.2	5413.2	10.5229
1300	72.6038	4687.4	5413.4	11.5857										
$P = 0.20\text{MPa}$ (120.3)					$P = 0.30\text{MPa}$ (133.5)					$P = 0.40\text{MPa}$ (143.6)				
$T(^{\circ}\text{C})$	$V(\text{m}^3/\text{kg})$	$U(\text{kJ}/\text{kg})$	$H(\text{kJ}/\text{kg})$	$S(\text{kJ}/\text{kg}\cdot\text{K})$	$T(^{\circ}\text{C})$	$V(\text{m}^3/\text{kg})$	$U(\text{kJ}/\text{kg})$	$H(\text{kJ}/\text{kg})$	$S(\text{kJ}/\text{kg}\cdot\text{K})$	$T(^{\circ}\text{C})$	$V(\text{m}^3/\text{kg})$	$U(\text{kJ}/\text{kg})$	$H(\text{kJ}/\text{kg})$	$S(\text{kJ}/\text{kg}\cdot\text{K})$
120.3	0.8857	2529.1	2706.2	7.1269	133.5	0.6058	2543.2	2724.9	6.9916	143.6	0.4624	2553.1	2738.1	6.8955
150	0.9599	2577.1	2769.1	7.2810	150	0.6340	2571.0	2761.2	7.0791	150	0.4709	2564.4	2752.8	6.9306
200	1.0805	2654.6	2870.7	7.5081	200	0.7164	2651.0	2865.9	7.3131	200	0.5343	2647.2	2860.9	7.1723
250	1.1989	2731.4	2971.2	7.7100	250	0.7964	2728.9	2967.9	7.5180	250	0.5952	2726.4	2964.5	7.3804
300	1.3162	2808.8	3072.1	7.8941	300	0.8753	2807.0	3069.6	7.7037	300	0.6549	2805.1	3067.1	7.5677
350	1.4330	2887.3	3173.9	8.0644	350	0.9536	2885.9	3172.0	7.8750	350	0.7140	2884.4	3170.0	7.7399
400	1.5493	2967.1	3277.0	8.2236	400	1.0315	2966.0	3275.5	8.0347	400	0.7726	2964.9	3273.9	7.9002
450	1.6655	3048.5	3381.6	8.3734	450	1.1092	3047.5	3380.3	8.1849	450	0.8311	3046.6	3379.0	8.0508
500	1.7814	3131.4	3487.7	8.5152	500	1.1867	3130.6	3486.6	8.3271	500	0.8894	3129.8	3485.5	8.1933
550	1.8973	3215.9	3595.4	8.6502	550	1.2641	3215.3	3594.5	8.4623	550	0.9475	3214.6	3593.6	8.3287
600	2.0130	3302.2	3704.8	8.7792	600	1.3414	3301.6	3704.0	8.5914	600	1.0056	3301.0	3703.2	8.4580
650	2.1287	3390.2	3815.9	8.9030	650	1.4186	3389.7	3815.3	8.7153	650	1.0636	3389.1	3814.6	8.5820
700	2.2443	3479.9	3928.8	9.0220	700	1.4958	3479.5	3928.2	8.8344	700	1.1215	3479.0	3927.6	8.7012
750	2.3599	3571.4	4043.4	9.1369	750	1.5729	3571.0	4042.9	8.9494	750	1.1794	3570.6	4042.4	8.8162
800	2.4755	3664.7	4159.8	9.2479	800	1.6500	3664.3	4159.3	9.0604	800	1.2373	3663.9	4158.8	8.9273
850	2.5910	3759.6	4277.8	9.3555	850	1.7271	3759.3	4277.4	9.1680	850	1.2951	3759.0	4277.0	9.0350
900	2.7066	3856.3	4397.6	9.4598	900	1.8042	3856.0	4397.3	9.2724	900	1.3530	3855.7	4396.9	9.1394
950	2.8221	3954.7	4519.1	9.5612	950	1.8812	3954.4	4518.8	9.3739	950	1.4108	3954.2	4518.5	9.2409
1000	2.9375	4054.8	4642.3	9.6599	1000	1.9582	4054.5	4642.0	9.4726	1000	1.4686	4054.3	4641.7	9.3396
1050	3.0530	4156.4	4767.0	9.7560	1050	2.0352	4156.2	4766.7	9.5687	1050	1.5264	4155.9	4766.5	9.4357
1100	3.1685	4259.6	4893.3	9.8497	1100	2.1122	4259.4	4893.1	9.6624	1100	1.5841	4259.2	4892.8	9.5295
1150	3.2839	4364.3	5021.1	9.9411	1150	2.1892	4364.1	5020.9	9.7538	1150	1.6419	4363.9	5020.7	9.6209
1200	3.3994	4470.5	5150.4	10.0304	1200	2.2662	4470.3	5150.2	9.8431	1200	1.6997	4470.1	5150.0	9.7102
1250	3.5148	4578.1	5281.1	10.1176	1250	2.3432	4577.9	5280.9	9.9303	1250	1.7574	4577.8	5280.7	9.7975
1300	3.6302	4687.0	5413.1	10.2029	1300	2.4202	4686.9	5412.9	10.0156	1300	1.8152	4686.7	5412.8	9.8828

**ANSWERS: Chemical Engineering Thermodynamics
Quiz 1 January 14, 2016**

1)

P1.1. Estimate the average speed (mph) of hydrogen molecules at 200 K and 3 bars.

H₂ is 2.02 g/mole

R = 8.314 J/(K mole)

Joule = kg m²/s²

2.24 mph/(m/s)

You can assume you know the temperature and pressure to 10% accuracy or you can make some other assumption concerning the accuracy of these values (state your assumption).

$$\text{Energy} = 3/2 kT = 1/2 mv^2$$

So $v \sim (3RT/M_w)^{1/2} = \mathbf{3500 \text{ mph}}$ if you assume 10% accuracy in the temperature and you assume an ideal gas. The ideal gas assumption is probably not very good at 3 bar. You don't need the pressure if you assume an ideal gas. The book answer seems to be wrong.

2)

1.12. The gas phase reaction $A \rightarrow 2R$ is conducted in a 0.1 m³ spherical tank. The initial temperature and pressure in the tank are 0.05 MPa and 400 K. After species A is 50% reacted, the temperature has fallen to 350 K. What is the pressure in the vessel?

$$R = 8.314 \text{ cm}^3 \text{ MPa}/(\text{K mole})$$

Initially assume you are at pure "A"

Use the ideal gas law you can get the initial moles of "A"

$$n_{A,i} = PV/RT = 0.05 \text{ MPa } 0.1 \times 10^6 \text{ cm}^3 / (8.314 \text{ (cm}^3 \text{ MPa}/(\text{K mole})) 400\text{K})$$

=1.5 moles of A initially

Then 50% reacts so you have 0.75 moles of A and 1.50 moles of R so you have 2.25 moles total.

Again assume an ideal gas (doesn't matter the type of atom for an ideal gas)

$$P = n_{\text{total}}RT/V = 2.25 \text{ moles } 8.314 \text{ (cm}^3 \text{ MPa}/(\text{K mole})) 400\text{K} / 0.1 \times 10^6 \text{ cm}^3 = \mathbf{0.075 \text{ MPa}}$$

assuming 10% accuracy in the initial values. He gets 0.065 in the book answer after a bit more complicated calculation.

3)

1.17. Determine the temperature, volume, and quality for one kg water under the following conditions:

a. $U = 3000 \text{ kJ/kg}, P = 0.3 \text{ MPa}$

c. $U = 2500 \text{ kJ/kg}, P = 0.3 \text{ MPa}$

(1.17) Determine the temperature, volume, and quality under the following conditions:

a) $U=3000, P=0.3 \Rightarrow$ superheated $q = 1, T = 400 + (3000-2966)/(3047.5-2966.0) * 50 = 421^\circ\text{C}$
 $V = 1.0315 + 21/50 * (1.1092-1.0315) = 1.064 \text{ m}^3/\text{kg}$

Assume 10% accuracy in the P and U values so you have $1.1 \text{ m}^3/\text{kg}$ (you can make other assumptions concerning the accuracy but need to state that.) It asks for one kg of water so the answer is **1.1 m^3 and 420°C** .

c) $U=2500, P=0.3 \Rightarrow$ two-phase, $T = 133.58^\circ\text{C}$
 $U = 2500 = 561. + q*1982.0, q = 0.978$
 $V = 0.001073 + 0.978 * (0.6058 - 0.001073) = 0.593 \text{ m}^3/\text{kg}$

Again, assume 10% accuracy in values he specifies for U and P so,
 $T = 130^\circ\text{C}, q = 0.98,$ and it is for 1 kg so 0.59 m^3 .