

Introductory Chemical Engineering Thermodynamics

CHAPTER 6

(6.01) CO₂ has two significant...

CO₂ has two significant vibrations at $\epsilon/k=952\text{K}$ that represent the axial stretches of both bonds. Other vibrations exist but at higher T .

(a) Plot C_v/R vs T for CO₂ in the range 200-400K. Include the polynomial as a dashed line and the NIST data as points. (b) What fraction of the IR spectrum does 903cm^{-1} comprise? (c) If absorption efficiency is proportional to concentration, what fraction of IR energy could be absorbed in this case.

Solution : a. For a linear ideal gas molecule, we must include the degrees of freedom for translation. (cf. HW4.1) Including only the given vibration (ignoring higher temperature vibrations), and adapting Eqn. 6.50,

$$C_v/R = 3/2(\text{translation}) + 2/2(\text{rotation about linear axis doesn't count}) + 2(2\text{symmetric bonds}) * (\beta\epsilon)^2 \exp(-\beta\epsilon) / [\exp(-\beta\epsilon) - 1]^2 + \dots (\text{higher vibs})$$

$$= 2.5 + 2 * (\beta\epsilon)^2 \exp(-\beta\epsilon) / [\exp(-\beta\epsilon) - 1]^2 \sim \text{off by ignoring higher vibs.}$$

| T(K) | 220 | 230 | 240 | 250 | 260 | 270 | 280 | 290 | 300 | 310 |
|-----------------------|------|------|------|------|------|------|------|------|------|------|
| $C_v/R(\text{nist})$ | 3.07 | 3.11 | 3.17 | 3.22 | 3.27 | 3.33 | 3.38 | 3.44 | 3.49 | 3.54 |
| $\beta\epsilon$ | 4.33 | 4.14 | 3.97 | 3.81 | 3.66 | 3.53 | 3.40 | 3.28 | 3.17 | 3.07 |
| $C_v/R(\text{calc})$ | 3.01 | 3.06 | 3.12 | 3.17 | 3.23 | 3.28 | 3.33 | 3.37 | 3.42 | 3.46 |
| C_v/R_{poly} | 3.02 | 3.08 | 3.14 | 3.20 | 3.26 | 3.32 | 3.37 | 3.43 | 3.48 | 3.53 |

| T(K) | 320 | 330 | 340 | 350 | 360 | 370 | 380 | 390 | 400 |
|-----------------------|------|------|------|------|------|------|------|------|------|
| $C_v/R(\text{nist})$ | 3.59 | 3.65 | 3.70 | 3.74 | 3.79 | 3.84 | 3.89 | 3.93 | 3.98 |
| $\beta\epsilon$ | 2.98 | 2.88 | 2.80 | 2.72 | 2.64 | 2.57 | 2.51 | 2.44 | 2.38 |
| $C_v/R(\text{calc})$ | 3.50 | 3.54 | 3.58 | 3.62 | 3.65 | 3.68 | 3.72 | 3.75 | 3.77 |
| C_v/R_{poly} | 3.59 | 3.64 | 3.69 | 3.74 | 3.78 | 3.83 | 3.88 | 3.92 | 3.97 |

b. IR runs from $12800\text{--}10\text{cm}^{-1}$, so 903 represents $1/12799=0.008\%$ of IR range.

c. $380\text{ppm} = 380/1\text{E}6 \Rightarrow 8\text{E-}9\%$ of IR could be absorbed by CO₂.

d. It is not unreasonable to ask questions about global warming by CO₂.

(6.02) Express in terms of P , V , T , C_p , C_v , and their derivatives. Your answer may include absolute values of S if it is not associated with a derivative.

a. $(\partial G/\partial P)_T = (\partial H/\partial P)_T - T(\partial S/\partial P)_T = [V - T(\partial V/\partial T)_P] + T(\partial V/\partial T)_P = V$ or using expansion rule:

$$(\partial G/\partial P)_T = -S(\partial T/\partial P)_T + V(\partial P/\partial P)_T = V \quad (6.7)$$

$$b. (\partial A / \partial P)_V = -S(\partial T / \partial P)_V - P(\partial V / \partial P)_V = -S(\partial T / \partial P)_V \Rightarrow (\partial P / \partial A)_V = -(\partial P / \partial T)_V / S$$

$$c. (\partial T / \partial P)_S = \frac{T}{C_p} \left(\frac{\partial V}{\partial T} \right)_P \quad (6.37)$$

$$\text{or, by triple product rule: } \left(\frac{\partial T}{\partial P} \right)_S = - \left(\frac{\partial T}{\partial S} \right)_P \left(\frac{\partial S}{\partial P} \right)_T = \frac{T}{C_p} \left(\frac{\partial V}{\partial T} \right)_P$$

$$d. H = U + PV \Rightarrow \left(\frac{\partial H}{\partial T} \right)_U = \left(\frac{\partial U}{\partial T} \right)_U + V \left(\frac{\partial P}{\partial T} \right)_U + P \left(\frac{\partial V}{\partial T} \right)_U = V \left(\frac{\partial P}{\partial T} \right)_U + \left[T \left(\frac{\partial P}{\partial T} \right)_V - P \right]$$

$$(\partial P / \partial T)_U = -(\partial U / \partial T)_P / (\partial U / \partial P)_T \quad \text{TPR} \quad (6.41)$$

$$(\partial U / \partial T)_P = C_V (\partial T / \partial T)_P + [T(\partial P / \partial T)_V - P](\partial V / \partial T)_P \quad (6.41)$$

$$(\partial U / \partial P)_T = C_V (\partial T / \partial P)_T + [T(\partial P / \partial T)_V - P](\partial V / \partial P)_T$$

$$\Rightarrow \left(\frac{\partial P}{\partial T} \right)_U = - \frac{C_V + [T(\partial P / \partial T)_V - P](\partial V / \partial T)_P}{[T(\partial P / \partial T)_V - P](\partial V / \partial P)_T}$$

$$\left(\frac{\partial H}{\partial T} \right)_U = -V \left(\frac{C_V + [T(\partial P / \partial T)_V - P](\partial V / \partial T)_P}{[T(\partial P / \partial T)_V - P](\partial V / \partial P)_T} \right) + \left[T \left(\frac{\partial P}{\partial T} \right)_V - P \right]$$

alt: starting with H(T,P), then applying the expansion

$$\text{rule: } \left(\frac{\partial H}{\partial T} \right)_U = C_p \left(\frac{\partial T}{\partial T} \right)_U + \left[V - T \left(\frac{\partial V}{\partial T} \right)_P \right] \left(\frac{\partial P}{\partial T} \right)_U \quad (6.40)$$

Insert for $(\partial P / \partial T)_U$ as determined above:

$$\Rightarrow \left(\frac{\partial H}{\partial T} \right)_U = C_p - \left[V - T \left(\frac{\partial V}{\partial T} \right)_P \right] \left\{ \frac{C_V + [T(\partial P / \partial T)_V - P](\partial V / \partial T)_P}{[T(\partial P / \partial T)_V - P](\partial V / \partial P)_T} \right\}$$

Note the relation between C_p and C_v can be inserted for answers that look different.

Note another expression for the last term on the first line:

$$\frac{PC_V}{T(\partial P / \partial T)_V - P} = \frac{P(C_p - T(\partial P / \partial T)_V (\partial V / \partial T)_P)}{T(\partial P / \partial T)_V - P}$$

$$e. (\partial H / \partial T)_S = T(\partial S / \partial T)_S + V(\partial P / \partial T)_S = -V(\partial S / \partial T)_P (\partial P / \partial S)_T = V \frac{C_p}{T} \left(\frac{\partial T}{\partial V} \right)_P;$$

$$(\partial H / \partial T)_S = \frac{T}{VC_p} \left(\frac{\partial V}{\partial T} \right)_P \text{ using (6.5 + 6.37), } (\partial T / \partial H)_S = \frac{T}{VC_p} \left(\frac{\partial V}{\partial T} \right)_P$$

$$f. \text{ expansion rule } (\partial A / \partial V)_P = -S(\partial T / \partial V)_P - P(\partial V / \partial V)_P = -S(\partial T / \partial V)_P - P \quad (6.6)$$

$$g. (\partial T / \partial P)_H = -\frac{1}{C_p} \left[V - T \left(\frac{\partial V}{\partial T} \right)_P \right] \text{ (cf. eqn. 6.40)}$$

$$\text{or by triple product rule, } \left(\frac{\partial T}{\partial P} \right)_H = - \left(\frac{\partial T}{\partial H} \right)_P \left(\frac{\partial H}{\partial P} \right)_T = -\frac{1}{C_p} \left(\frac{\partial H}{\partial P} \right)_T = -\frac{1}{C_p} \left[V - T \left(\frac{\partial V}{\partial T} \right)_P \right]$$

$$h. (\partial A / \partial S)_P = -S(\partial T / \partial S)_P - P(\partial V / \partial S)_P = -ST / C_p - P(\partial V / \partial S)_P \quad (6.6 + 6.37)$$

$$(\partial V / \partial S)_P = T / C_p (\partial V / \partial T)_P \quad (6.39)$$

$$(\partial A / \partial S)_P = -T [S + P(\partial V / \partial T)_P] / C_p$$

$$\begin{aligned}
 (\partial S/\partial P)_G &= -(\partial G/\partial P)_S/(\partial G/\partial S)_P && \text{TPR} \\
 \text{expansion rule } (\partial G/\partial P)_S &= -S(\partial T/\partial P)_S + V(\partial P/\partial P)_S = && (6.7) \\
 (\partial T/\partial P)_S &= \frac{T}{C_P} \left(\frac{\partial V}{\partial T} \right)_P && (6.37) \\
 \text{expansion rule } (\partial G/\partial S)_P &= -S(\partial T/\partial S)_P + V(\partial P/\partial S)_P = -ST/C_P && (6.7 + 6.37) \\
 (\partial S/\partial P)_G &= [-S(\partial T/\partial P)_S + V]/[-ST/C_P] = C_P [-S(\partial T/\partial P)_S + V]/[ST] \\
 &= \frac{C_P \left[\frac{-ST}{C_P} \left(\frac{\partial V}{\partial T} \right)_P + V \right]}{ST} = \frac{VC_P}{ST} - \left(\frac{\partial V}{\partial T} \right)_P
 \end{aligned}$$

(6.03) Derive in terms of U, H, S, G, S, P, V, T and their derivatives.

$$\left(\frac{\partial(G/RT)}{\partial T} \right)_P = \frac{1}{RT} \left(\frac{\partial G}{\partial T} \right)_P - \frac{G}{RT^2} = \frac{-S}{RT} - \left(\frac{H}{RT^2} - \frac{S}{RT} \right) = \frac{-S}{RT} + \frac{S}{RT} - \frac{H}{RT^2} = -\frac{H}{RT^2}$$

FYI: We can rearrange these as:

$$\beta \equiv 1/RT \Rightarrow d\beta/dT = -1/RT^2 = -\beta/T \Rightarrow d\beta/\beta = -dT/T.$$

$$T \left(\frac{\partial(A/RT)}{\partial T} \right)_V = -\frac{U}{RT} = -\beta \left(\frac{\partial(\beta A)}{\partial \beta} \right)_V \Rightarrow A/RT = \int \frac{U}{RT} \frac{d\beta}{\beta}$$

$$T \left(\frac{\partial(G/RT)}{\partial T} \right)_P = -\frac{H}{RT} = -\beta \left(\frac{\partial(\beta G)}{\partial \beta} \right)_P$$

Thus transformations between U and A are quick (and common).

(6.04) Derive $(dH/dP)_T$ and $(dU/dP)_T$ in terms of measurable properties...

a. Starting with U, H and applying expansion rule.

$$\left(\frac{\partial U}{\partial P} \right)_T = T \left(\frac{\partial S}{\partial P} \right)_T - P \left(\frac{\partial V}{\partial P} \right)_T = -T \left(\frac{\partial V}{\partial T} \right)_P - P \left(\frac{\partial V}{\partial P} \right)_T$$

$$\left(\frac{\partial H}{\partial P} \right)_T = T \left(\frac{\partial S}{\partial P} \right)_T + V \left(\frac{\partial P}{\partial P} \right)_T = -T \left(\frac{\partial V}{\partial T} \right)_P + V$$

b. Taking difference of result of part a.

$$\left(\frac{\partial H}{\partial P} \right)_T - \left(\frac{\partial U}{\partial P} \right)_T = V + P \left(\frac{\partial V}{\partial P} \right)_T$$

Applying Expansion Rule

$$\left(\frac{\partial H}{\partial P} \right)_T = \left(\frac{\partial U}{\partial P} \right)_T + \left(\frac{\partial(PV)}{\partial P} \right)_T$$

$$\left(\frac{\partial H}{\partial P} \right)_T = \left(\frac{\partial U}{\partial P} \right)_T + P \left(\frac{\partial V}{\partial P} \right)_T + V \left(\frac{\partial P}{\partial P} \right)_T = \left(\frac{\partial U}{\partial P} \right)_T + P \left(\frac{\partial V}{\partial P} \right)_T + V$$

The desired difference is the same.

(6.05) In Chapter 2, internal energy of condensed phases....

a. Starting with U, H and applying expansion rule.

$$\left(\frac{\partial U}{\partial P}\right)_T = T\left(\frac{\partial S}{\partial P}\right)_T - P\left(\frac{\partial V}{\partial P}\right)_T = -T\left(\frac{\partial V}{\partial T}\right)_P - P\left(\frac{\partial V}{\partial P}\right)_T = -TV\alpha_p + PV\kappa_T$$

$$\left(\frac{\partial H}{\partial P}\right)_T = T\left(\frac{\partial S}{\partial P}\right)_T + V\left(\frac{\partial P}{\partial P}\right)_T = -T\left(\frac{\partial V}{\partial T}\right)_P + V = -TV\alpha_p + V$$

| | | | | | |
|------------------|--------|---------|--------------------|-----------|-----------|
| P = | 0.1 | MPa | | | |
| T = | 293 | K | | | |
| Liquid | MW | rho | 1E3 alpha | 1E6*kappa | V |
| | | (g/cm3) | (K ⁻¹) | (bar-1) | (cm3/mol) |
| Acetone | 58.08 | 0.7899 | 1.487 | 111 | 73.528295 |
| Ethanol | 46.07 | 0.7893 | 1.12 | 100 | 58.368174 |
| Benzene | 78.12 | 0.87865 | 1.237 | 89 | 88.909122 |
| Carbon disulfide | 76.14 | 1.258 | 1.218 | 86 | 60.524642 |
| Chloroform | 119.38 | 1.4832 | 1.273 | 83 | 80.488134 |
| Ethyl ether | 74.12 | 0.7138 | 1.656 | 188 | 103.83861 |
| Mercury | 200.6 | 13.5939 | 0.18186 | 3.95 | 14.756619 |
| Water | 18.02 | 0.998 | 0.207 | 49 | 18.056112 |

Note: Since J is given by (cm3MPa/mol), then (cm3/mol) is J/MPa

| Liquid | -T(dV/dT)P | -P(dV/dP)T | (dU/dP)T | (dH/dP)T |
|------------------|------------|------------|----------|----------|
| | (cm3/mol) | (cm3/mol) | J/MPa | J/MPa |
| Acetone | -32.0356 | 0.081616 | -31.954 | 41.49268 |
| Ethanol | -19.1541 | 0.058368 | -19.0957 | 39.21407 |
| Benzene | -32.2243 | 0.079129 | -32.1452 | 56.68481 |
| Carbon disulfide | -21.5997 | 0.052051 | -21.5476 | 38.92497 |
| Chloroform | -30.0212 | 0.066805 | -29.9544 | 50.46695 |
| Ethyl ether | -50.3833 | 0.195217 | -50.1881 | 53.45529 |
| Mercury | -0.78631 | 0.000583 | -0.78572 | 13.97031 |
| Water | -1.09512 | 0.008847 | -1.08627 | 16.96099 |

The derivatives are larger for organics than for mercury and water. Molar volume is the largest contribution to $(dH/dP)_T$, especially for water and mercury. The coefficient of thermal expansion is most important in determining $(dU/dP)_T$.

(6.06) Express $(dH/dV)_T$ in terms of ...

$$dH = TdS + VdP$$

$$\left(\frac{\partial H}{\partial V}\right)_T = T\left(\frac{\partial S}{\partial V}\right)_T + V\left(\frac{\partial P}{\partial V}\right)_T$$

$$= T\left(\frac{\partial P}{\partial T}\right)_V + V\left(\frac{\partial P}{\partial V}\right)_T \quad \text{where} \quad \left(\frac{\partial P}{\partial T}\right)_V = -\left(\frac{\partial V}{\partial T}\right)_P \left(\frac{\partial P}{\partial V}\right)_T = \frac{\alpha_p}{\kappa_T}$$

$$= \frac{\alpha_p T - 1}{\kappa_T}$$

(6.07) Express the adiabatic compressibility...

First use triple product rule

$$k_s = \frac{1}{V} \left(\frac{\partial V}{\partial S} \right)_P \left(\frac{\partial S}{\partial P} \right)_V$$

now interpose temperature using chain rule, because temperature derivatives of S are heat capacities.

$$\begin{aligned} k_s &= \frac{1}{V} \left[\left(\frac{\partial V}{\partial T} \right)_P \left(\frac{\partial T}{\partial S} \right)_P \right] \left[\left(\frac{\partial S}{\partial T} \right)_V \left(\frac{\partial T}{\partial P} \right)_V \right] \\ &= \frac{1}{V} \frac{C_V}{C_P} \left(\frac{\partial V}{\partial T} \right)_P \left(\frac{\partial T}{\partial P} \right)_V \end{aligned}$$

Now, using triple product rule on last two derivatives

$$k_s = -\frac{1}{V} \frac{C_V}{C_P} \left(\frac{\partial V}{\partial P} \right)_T = \frac{C_V}{C_P} k_T$$

(6.08) Express the Joule-Thomson coefficient in terms of measurable ...

(a) Van der Waals equation given in Example 6.6

(b) An ideal gas.

$$\left(\frac{\partial T}{\partial P} \right)_H = \frac{-1}{C_P} \left[V - T \left(\frac{\partial V}{\partial T} \right)_P \right] \quad (6.40)$$

a. $P = RT/(V-b) - a/V^2$. $\Rightarrow P(V-b) = RT - a(V-b)/V^2$. Differentiating implicitly,

$$P(\partial V/\partial T)_P = -a(\partial V/\partial T)_P [1/V^2 - 2(V-b)/V^3]$$

$$\Rightarrow (\partial V/\partial T)_P = 1/(P + a[1/V^2 - 2(V-b)/V^3]) = V^3/[PV^3 + aV - 2a(V-b)]$$

$$\text{Alt. } PV^2 = RTV^2/(V-b) - a \Rightarrow 2PV(\partial V/\partial T)_P = (\partial V/\partial T)_P [RT2V/(V-b) + RTV^2/(V-b)^2].$$

$$(\partial V/\partial T)_P = 1/[2PV - 2RTV/(V-b) - RTV^2/(V-b)^2] = (V-b)^2/[2P(V-b)^2 - 2RTV(V-b) - RTV^2]$$

b. $PV = RT \Rightarrow (\partial V/\partial T)_P = RT/P = V \Rightarrow (\partial T/\partial P)_H = 0$.

(6.09) Prove $(\partial P/\partial T)_S = \dots$

$$\left(\frac{\partial P}{\partial T} \right)_S = \frac{C_P}{TV \left(\frac{1}{V} \left(\frac{\partial V}{\partial T} \right)_P \right)}$$

a)

$$= \frac{C_P}{T} \left(\frac{\partial T}{\partial V} \right)_P$$

Rearranging:

$$\left(\frac{\partial P}{\partial T} \right)_S \left(\frac{\partial V}{\partial T} \right)_P = \frac{C_P}{T} = \left(\frac{\partial S}{\partial T} \right)_P$$

By Maxwell

$$\left(\frac{\partial V}{\partial T} \right)_P = - \left(\frac{\partial S}{\partial P} \right)_T$$

plugging back in,

$$-\left(\frac{\partial P}{\partial T}\right)_S \left(\frac{\partial S}{\partial P}\right)_T = \left(\frac{\partial S}{\partial T}\right)_P$$

This is just triple product rule, proof complete.

$$b) \frac{P}{P^i} = \left(\frac{T}{T^i}\right)^{\frac{C_p}{R}}$$

$$\left(\frac{\partial P}{\partial T}\right)_S = P^i \left(\frac{1}{T^i}\right)^{\frac{C_p}{R}} \frac{C_p}{R} T^{\left(\frac{C_p}{R}-1\right)} = \frac{C_p P^i T^{\frac{C_p}{R}}}{R (T^i)^{\frac{C_p}{R}}}$$

$$\text{note: } \frac{P}{P^i} = \left(\frac{T}{T^i}\right)^{\frac{C_p}{R}} \Rightarrow \frac{P^i}{(T^i)^{C_p/R}} = \frac{P}{T^{C_p/R}}$$

$$\left(\frac{\partial P}{\partial T}\right)_S = \frac{C_p P}{R T^{(C_p-C_v)/R}} = \frac{C_p P}{R T}$$

Now, compare with result from part (a).

$$\left(\frac{\partial P}{\partial T}\right)_S = \frac{C_p}{T} \left(\frac{\partial T}{\partial V}\right)_P; \quad V = \frac{RT}{P}$$

$$\left(\frac{\partial V}{\partial T}\right)_P = \frac{R}{P}; \text{ plugging in results into part (a)}$$

$$\left(\frac{\partial P}{\partial T}\right)_S = \frac{C_p}{TV \left(\frac{1}{V} \frac{R}{P}\right)} = \frac{C_p P}{R T}$$

Results agree.

Note: there are many ways to do a proof that also might be correct.

(6.10) Determine the difference....

| Liquid | MW | rho | 1E3 alpha (K ⁻¹) | 1E6* kappa (bar ⁻¹) | V (cm ³ /mol) | Cp- Cv J/mol-K |
|---------------------|--------|---------|------------------------------------|---------------------------------------|-----------------------------|----------------------|
| | | (g/cm3) | | | | |
| Acetone | 58.08 | 0.7899 | 1.487 | 111 | 73.53 | 42.9 |
| Ethanol | 46.07 | 0.7893 | 1.12 | 100 | 58.37 | 21.45 |
| Benzene | 78.12 | 0.8787 | 1.237 | 89 | 88.91 | 44.79 |
| Carbon disulfide | 76.14 | 1.258 | 1.218 | 86 | 60.52 | 30.59 |
| Chloroform | 119.38 | 1.4832 | 1.273 | 83 | 80.49 | 46.04 |
| Ethyl ether | 74.12 | 0.7138 | 1.656 | 188 | 103.84 | 44.38 |
| Mercury | 200.6 | 13.594 | 0.1819 | 3.95 | 14.76 | 3.62 |
| Water | 18.02 | 0.998 | 0.207 | 49 | 18.06 | 0.46 |

| Liquid | A | B | C | T | Cp J/mol-K |
|---------|--------|-----------|----------|-----|---------------|
| Acetone | | | | | |
| Ethanol | 33.866 | -1.73E-01 | 3.49E-04 | 293 | 110.3276 |

| | | | | | |
|------------------|--------|-----------|-----------|-----|----------|
| Benzene | -0.747 | 6.80E-02 | -3.78E-05 | 293 | 132.3747 |
| Carbon disulfide | | | | | |
| Chloroform | 19.215 | -4.29E-02 | 8.30E-05 | 293 | 114.5217 |
| Ethyl ether | | | | | |
| Mercury | | | | | |
| Water | 8.712 | 1.25E-03 | 1.08E-07 | 293 | 75.55366 |

(6.11) A rigid container is filled with liquid acetone...

$$a) \left(\frac{\partial P}{\partial T} \right)_V = - \left(\frac{\partial P}{\partial V} \right)_T \left(\frac{\partial V}{\partial T} \right)_P = \frac{1.478 \times 10^{-3}}{111 \times 10^{-6}} = 13.4 \text{ bar/}^\circ\text{C}$$

$$100 \text{ bar} / (13.4 \text{ bar/}^\circ\text{C}) = 7.5 \text{ }^\circ\text{C}$$

$$b) C_P - C_V = T \left(\frac{\partial P}{\partial T} \right)_V \left(\frac{\partial V}{\partial T} \right)_P = -T \left(\frac{\partial P}{\partial V} \right)_T \left(\frac{\partial V}{\partial T} \right)_P^2$$

$$C_V = C_P + T \left(\frac{\partial P}{\partial V} \right)_T \left(\frac{\partial V}{\partial T} \right)_P^2 = C_P - TV \frac{\alpha_P^2}{\kappa_T}$$

$$= 125 - (293)(73.5) \frac{(1.487 \times 10^{-3})^2}{111 \times 10^{-6}} \text{ (J/(10 bar cm}^3\text{))} = 82 \text{ J/mol K}$$

$$\Delta U = \int C_V dT = (82)(7.5) = 615 \text{ J/mol}$$

Liquid is incompressible,

$$\Delta H = \Delta U + \Delta(PV) = \Delta U + V\Delta P = 615 + \frac{73.5(100)}{10} = 1350 \text{ J/mol}$$

Alternatively

$$\Delta H = \int \left(\frac{\partial H}{\partial T} \right)_V dT$$

Expansion Rule:

$$\left(\frac{\partial H}{\partial T} \right)_V = T \left(\frac{\partial S}{\partial T} \right)_V + V \left(\frac{\partial P}{\partial T} \right)_T$$

$$= C_V - V \left(\frac{\partial P}{\partial V} \right)_T \left(\frac{\partial V}{\partial T} \right)_P = C_V + V \frac{\alpha_P}{\kappa_T}$$

$$= 82 + (73.5 \text{ cm}^3)(1.487 \times 10^{-3} \text{ bar}) / (111 \times 10^{-6}) / (10 \text{ cm}^3 \text{ bar/J}) = 180 \text{ J/mol K}$$

$$\Delta H = \int 180 dT = 180(7.5) = 1350 \text{ J/mol}$$

$$\Delta S = \left(\frac{\partial S}{\partial T} \right)_V dT = C_V \ln \frac{T_2}{T_1} = 82 \ln \frac{300.5}{293} = 2.07 \text{ J/mol K}$$

Note: These answers are different from those obtained by constant pressure heating where $\Delta U \approx \Delta H$.

$$c) \Delta U = Q = 615 \text{ J/mol}$$

(6.12) The fundamental internal energy relation for a rubber band is...

(a) we seek $\left(\frac{\partial T}{\partial L}\right)_S$, which we should be able to find in terms of other derivatives.

Using the triple product rule, $\left(\frac{\partial T}{\partial L}\right)_S = -\left(\frac{\partial T}{\partial S}\right)_L \left(\frac{\partial S}{\partial L}\right)_T = -\frac{T}{C_L} \left(\frac{\partial S}{\partial L}\right)_T$.

Now, C_L must be positive, let us explore $\left(\frac{\partial S}{\partial L}\right)_T$. The fluid analog of this derivative is $\left(\frac{\partial S}{\partial V}\right)_T$

which we find as a Maxwell from the Helmholtz energy. Defining an analog of the Helmholtz energy, $A' = U - TS$, $dA' = dU - TdS - SdT = -SdT - FdL$. The cross derivatives result in the relation that we are seeking:

$\left(\frac{\partial S}{\partial L}\right)_T = \left(\frac{\partial F}{\partial T}\right)_L$, and the temperature dependence of F is given, but must be analyzed carefully

since F_{applied} is given. $F = -F_{\text{applied}} = -k(T)(L-L_0)$, and since $k(T)$ increases with T , then F

decreases with T at fixed L , meaning, $\left(\frac{\partial S}{\partial L}\right)_T < 0$. therefore, $\left(\frac{\partial T}{\partial L}\right)_S > 0$, so the temperature of

the rubber band rises when you do work on it by stretching it quickly. (Note that you do work on the rubber band by stretching, whereas you do work on a fluid by compressing).

(b) If we can find $\left(\frac{\partial L}{\partial T}\right)_F$ then we will have the sign.

Again starting with the triple product rule, $\left(\frac{\partial L}{\partial T}\right)_F = -\left(\frac{\partial L}{\partial F}\right)_T \left(\frac{\partial F}{\partial T}\right)_L$. Both derivatives on the

right hand side are easy to determine since the force law is given, $\left(\frac{\partial F}{\partial L}\right)_T < 0$, and we already

determined, $\left(\frac{\partial F}{\partial T}\right)_L < 0$, therefore $\left(\frac{\partial L}{\partial T}\right)_F < 0$. Therefore length goes down when T goes up, and

length goes up when T goes down, in other words, the rubber band is easier to stretch a given length at lower T . (Put one in the freezer and try it!) Note: it is possible to answer this question by just looking at the force law without using the derivatives).

(c) Perform an analog of example 5.10.

$dS = \left(\frac{\partial S}{\partial T}\right)_L dT + \left(\frac{\partial S}{\partial L}\right)_T dL$, using the expansion rule for T with respect to F ,

$$\left(\frac{\partial S}{\partial T}\right)_F = \left(\frac{\partial S}{\partial T}\right)_L \left(\frac{\partial T}{\partial T}\right)_F + \left(\frac{\partial S}{\partial L}\right)_T \left(\frac{\partial L}{\partial T}\right)_F$$

$$C_F = C_L + T \left(\frac{\partial S}{\partial L}\right)_T \left(\frac{\partial L}{\partial T}\right)_F \Rightarrow C_F - C_L = T \left(\frac{\partial S}{\partial L}\right)_T \left(\frac{\partial L}{\partial T}\right)_F, \text{ and } \left(\frac{\partial S}{\partial L}\right)_T < 0 \text{ from part (a), and}$$

$$\left(\frac{\partial L}{\partial T}\right)_F < 0 \text{ from part (b), therefore, } C_F - C_L > 0.$$

(d) $dQ = C_L dT_L = C_F dT_F$, Since $C_F > C_L$, $dT_L > dT_F$.

(c) In part (a) we analyzed $\left(\frac{\partial S}{\partial L}\right)_T = \left(\frac{\partial F}{\partial T}\right)_L$ and found it less than zero. This is because a rubber band is made from molecular strands which are like molecular spaghetti when processed and all tangled. When you pull on it, it aligns some of the molecules, and the entropy goes down. That is why the force law seems non-intuitive at first.

CHAPTER 7

(7.1) The compressibility factor chart provides:

at $Pr = 0.86$, the T range was $0.44 < T < 1.13$, $T = 12.1$

at $Pr = 0.41$, the T range was $0.403 < T < 1.4$, $T = 0.804$

at $Pr = 0.47$, the T range was $0.409 < T < 1.3$, $T = 0.75K$

Therefore, I can use van der Waals T and V for the vapor phase $Z = 0.4$ which the Red system is valid for all fluids the temperature is above T_{cr} .

(7.2) A container having a volume of 40 L...

given (i) methane

methane MW = 16, $T = 12.1$

initial state, $P = 2.172$, $Z = 0.4$, $Z_{cr} = 0.274$, $Z_{cr} = 0.274$, $Z_{cr} = 0.4$

$P = ZRT/P = 0.7 \text{ cm}^3/\text{mol}$

$m_{\text{gas}} = MW \cdot V/V = 3.62 \text{ kg}$

final state, $Pr = 1.24/2 = 0.62$, $Z = 0.4$, $Z_{cr} = 0.274$, $Z_{cr} = 0.4$

$P = ZRT/P = 0.342 \text{ cm}^3/\text{mol}$

$m_{\text{gas}} = MW \cdot V/V = 1.04 \text{ kg}$

1.04 kg lost

methane MW = 16, $T = 12.1$

Current State

$P = 2.172$, $Z = 0.4$, $Z_{cr} = 0.274$, $Z_{cr} = 0.4$

$P = 0.7 \text{ cm}^3/\text{mol}$

$m_{\text{gas}} = MW \cdot V/V = 3.62 \text{ kg}$

$m_{\text{gas}} = MW \cdot V/V = 3.62 \text{ kg}$

final state

Current State

$P = 0.342$, $Z = 0.4$, $Z_{cr} = 0.274$, $Z_{cr} = 0.4$

$P = 0.342 \text{ cm}^3/\text{mol}$

$m_{\text{gas}} = MW \cdot V/V = 1.04 \text{ kg}$

$m_{\text{gas}} = 1.04 \text{ kg}$

1.04 kg lost