Polymers



Figure 1. 50,000 setp Gaussian (left), 50,000 step SAW/SRI 1 cell (middle), 50,000 step SAW with 3 cell avoidance and 1 cell SRI (right). $50,000^{3/5} = 660$ and $50,000^{0.5} = 224$. End-to-end distance for the Gaussian is 71, for the SAW (1 step avoidance) is 397 and for 3 step avoidance is about 5000.



Figure 2. R end-to-end distance versus N in a log-log plot showing lines for 1/2 and 5/3 slope.

Polymers



Figure 2. R end-to-end distance versus N in a log-log plot showing lines for 1/2 and 5/3 slope.



If we consider a series of chains $\langle R \rangle = 0$

$$\langle R^2 \rangle = \sum_{i=1}^n \sum_{j=1}^n \langle r_i \cdot r_j \rangle = nr^2$$

$$r_i \bullet r_j = 0$$

Except when i = j, and there are "n" of these

 $r_i \bullet r_i = 1$

 $R_{RMS} = n^{1/2} \ell$

Similar to diffusion R ~ $Dt^{1/2}$

The distribution of chain lengths, R, follows almost a Gaussian Distribution:

$$P_G(x,\mu,\sigma) = \frac{1}{\sigma\sqrt{2\pi}} \exp\left[-\frac{1}{2}\left(\frac{x-\mu}{\sigma}\right)^2\right]$$

1-d Gaussian

$$P_G(R,n) = \frac{1}{\sqrt{2\pi nb^2}} \exp\left[-\frac{1}{2}\left(\frac{R}{b\sqrt{n}}\right)^2\right]$$

1-d Gaussian Walk of "n" steps

Boltzman Equation

$$P(R) = \exp\left(\frac{-E(R)}{kT}\right)$$

By Comparison

$$E(R) = \frac{3kTR^2}{2nl^2}$$

The energy of an ideal chain as a function of R

Energy of an Ideal Chain

$$E(R) = \frac{3kTR^2}{2nl^2}$$

$$F = \frac{dE(R)}{dR} = \frac{3kT}{nl^2}R = k_{spr}R$$

(Change in energy is force times the change in distance)

The modulus of rubber is proportional to temperature and inversely proportional to the molecular weight between crosslinks.



The ideal chain acts like a spring





Generally Modulus **decreases** with temperature

Polymer Chains are Mass-Fractals

 $R_{RMS} = n^{1/2} I$ Mass ~ Size²

3-d object Mass ~ Size³

2-d object Mass ~ Size²

I-d object Mass ~ Size¹

d_f-object

Mass ~ Size^{df}

 \sim d.

This leads to odd properties:

density
$$\rho = \frac{Mass}{Volume} = \frac{Mass}{Size^3} = \frac{Size^{d_f}}{Size^3} \sim Size^{d_f-3}$$

For a 3-d object density doesn't depend on size, For a 2-d object density drops with Size Larger polymers are less dense

Mass Fractal dimension, d_f



Random Aggregation (right) $d_f \sim 1.8$ Randomly Branched Gaussian $d_f \sim 2.3$ Self-Avoiding Walk $d_f = 5/3$

Problem:

Disk $d_f = 2$ Gaussian Walk $d_f = 2$



Nano-titania from Spray Flame

 $R/d_p = 10, z \sim 220$ $d_f = ln(220)/ln(10) = 2.3$



FIG. 1. Images of (a) balls folded from an aluminum sheet of thickness h=0.06 mm and edge size L=60 cm and (b) the cut through this ball. Balankin et al. (*Phys. Rev. E* **75** 051117

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A measure of topology is not given by d_f. Disk and coil are topologically different. Foil and disk are topologically similar.



Consider a Crumpled Sheet

A 2-d Sheet has c = 2 d_{min} depends on the extent of crumpling



 $d_f = 2.3$ $d_{\min} = 1.15$ c = 2

thickness h=0.06 mm and edge size L=60 cm and (b) the cut through this ball.

FIG. 1. Images of (a) balls folded from an aluminum sheet of



FIG. 3. (a) Data collapse for ρ/ρ_h versus R/h (the slope of the fitting line is 3-D=0.7009, $R^2=0.98$); and (b) log-log plot of ρ_h/ρ_m versus *h* (straight line is given by $y=1.728x^{-0.4816}$, $R^2=0.98$). Balankin et al. (*Phys. Rev. E* **75** 051117 (2007))



$$d_f = 2.3$$

 $d_{\min} = 1.47$
 $c = 1.56$





$$d_f = 2$$
$$d_{\min} = 1$$
$$c = 2$$

Extended β-sheet (misfolded protein)



Random Coil



Unfolded Gaussian chain



For a polymer in solution there is an inherent concentration to the chain since the chain contains some solvent



The polymer concentration is Mass/Volume, within a chain

$$c^* = \frac{Mass}{Volume} = \frac{Mass}{Size^3} = \frac{Size^{d_f}}{Size^3} \sim Size^{d_f - 3}$$
$$c^* \sim n^{\left(1 - 3/d_f\right)}$$

When the solution concentration matches c* the chains "overlap" Then an individual chain is can not be resolved and the chains entangle This is called a concentrated solution, the regime near c* is called semi-dilute and the regime below c* is called dilute



In concentrated solutions with chain overlap chain entanglements lead to a higher solution viscosity



J.R. Fried Introduction to Polymer Science

$$\eta \sim c^P$$

 $P = 1$ for c < c*

There is a similar behavior in Melt Viscosity as a function of Molecular Weight



 $\eta_0 \sim M^1$ for M < M_e $\eta_0 \sim M^{3.4}$ for M > M_e



M_e is the entanglement molecular weight about 10,000 g/mole (10 kDa)

FIGURE 3.6-4. Plots of constant + log η_c vs. constant + log M for nine different polymers. The two constants are different for each of the polymers, and the one appearing in the abscissa is proportional to concentration, which is constant for a given undiluted polymer. For each polymer the deps of the left and right straight line regions are 1.0 and 3.4, respectively. [G. C. Berry and T. G. Fox, Adv. Polym. Sci., 5, 261–357 (1968).]

Many Macromolecular Properties Change at Me

Onset of Shear Thinning Behavior in Rheology

Onset of Chain Folding Crystallization

Onset of Robust Mechanical Properties (Organic Powder versus Solid Plastic)

Onset of the ability to draw a fiber (melt strength)

Below the entanglement molecular weight we have an oligomer above we have a polymer or a plastic material



Figure 11.14. Effect of increasing molecular weight on the dependence of polymer viscosity on $\hat{\gamma}$ for polystyrene ($M_c = 31,200$) at 183°C. Molecular weights are (a) 242,000; (b) 217,000; (c) 179,000; (d) 117,000; and (e) 48,500. [Adapted from R. A. Stration, J. Colloid interface Sci., 22, 517 (1966), with permission of the publisher.]



Fig. 1-1 Dependence of melting temperatures, T_M , and boiling temperatures, T_{bp} , of alkanes and poly(methylene)s, H(CH₂)_NH, on the number N of methylene groups per molecule [1, 2].

From Hans-Georg Elias, Macromolecules 2005 ([2] = B. Wunderlich Macromolecular Physics vol. 3 1980)





and 90° ($\pi/2$) for Newtonian viscous behavoir We usually talk about tan δ that varies from 0 to ∞

Dynamic Mechanical Testing

A typical instrument for performing DMA can deform the sample in a number of different wa



Tension



















Hookean Elastic



Viscoelastic













Combine to make a master curve (Semi-Crystalline Polymer is Shown)



Can also combine frequencies for different temperatures

To yield a master curve in frequency



Time-Temperature Superposition

Temperature and Frequency Plots are directly related High Frequency => Low Temperature Low Frequency => High Temperature

Williams-Landel-Ferry Shift Factor, aT



 $\log[a_T] = C_1(T-T_{ref})/(C_2 + T - T_{ref})$

What is T dependence of shift factor?

Define: $a_T = t(T)/t_r(T_r)$ where t and t_r can be thought of as relaxation times log a _T = log t (T) - t_r (T_r) such that log a_T \clubsuit as TØ

Synthesis of Polymers

Polymers are generally produced by organic reactions similar to the organic chemistry you have studied except that the synthesis either involves a **Chain Reaction** generally with 3 stages

Initiation: You start the chain reaction

Propagation: You conduct the chain reaction

Termination: You end the chain reaction

Or it involves a **Step-Growth Reaction** where a simple reaction occurs at two (or more) ends of a growing chain molecule. This type of reaction involves di-functional (or higher functional) reactants. The reaction proceeds until you run out of reactants or the system becomes too viscous for transport of reacting species to the reacting chain ends.







- · Any two molecular species can react.
- Monomer disappears early.
- · Polymer MW rises throughout.
- · Growth of chains is usually slow (minutes to days).
- · Long reaction times increase MW, but yield of polymer hardly changes.
- · All molecular species are present throughout.
- Usually (but not always) polymer repeat unit has fewer atoms than had the monomer.

Chain Polymerization



- Growth occurs only by addition of monomer to active chain end.
- · Monomer is present throughout, but its concentration decreases.
- · Polymer begins to form immediately.
- · Chain growth is usually very rapid (second to microseconds).
- · MW and yield depend on mechanism details.
- · Only monomer and polymer are present during reaction.
- · Usually (but not always) polymer repeat unit has the same atoms as had the monomer

Carothers' Equations For Step Growth Polymerization





Chain Vs. Step Growth Polymerization

Chain Growth

A. Mechanism

Distinct and Different -Initiation Step -Propagation Steps -Termination Step(s)

B. Monomer Concentration

Monomer is present throughout the reaction, even at the end

C. Polymer Molecular Weight



Step Growth

Distinct and Different Initiation, Propagation and termination are all the same step "Termination" is the last reaction that takes place -Early in the reaction the monomer is depleted -Many dimers and trimers are produced early in the reaction. The monomer is consumed at early stages of the reaction



Reaction must be driven to 99.9% complete to get a polymer



Solution "A" (0.5 <u>M</u> hexamethylenediamine ($H_2N(CH_2)_6NH_2$, also called 1,6-diaminohexane) and 0.5 <u>M</u> sodium hydroxide in water), Solution "B" (0.2 <u>M</u> sebacoyl chloride ($ClOC(CH_2)_8COCl$) in hexane).

Nyon 6,10 by interfacial polymerization



Polyesters

Polycarbonate (CD's) bisphenol-A and phosgene





Terephthalic Acid and Ethylene glycol

Glyptal Synthesis



Pthalic Anhydride Glycerol (or Ethylene glycol)





+ (n - 1) NaCl



Gellation/Percolation

Carother's Method: Percolation occurs when $p=2/f_{avg}$

Example e For 2 A A + 3 B-B # A end groups (or B and groups) $f_{aug} = \frac{2(6)}{5} = 2.4$ Hof adole rulps $p_c = \frac{2}{2.4} = 83\%$

Polyurethane





When DABCO H-bonds with the alcohol, we're left with a partial positve charge on the nitrogen, and a partial negative charge on the oxygen.





Polyurethane



A step-reaction but **not** a condensation reaction.

There is no byproduct so this is a useful reaction for coatings and other systems where you do not want droplets of condensate.

Eventually these oligomers will merge and merge until we get high molecular weight polymer.



Finally, polyurethane

Polyurethane Foam



Step 1: A water molecule attacks the isocyanate carbon, giving us an ionic species.



Step 2: The isocyanate nitrogen swipes a hydrogen from the water.



Step 3: The nitrogen swipes *another* hydrogen, making an amine and carbon dioxide.



Step 4: The new amine attacks another isocyanate, just like the water attacked the old isocyanate.



Step 5: The nitrogen swipes a hydrogen from the amine, creating a urea linkage in the polymer.

Chain Vs. Step Growth Polymerization

Chain Growth

A. Mechanism

Distinct and Different -Initiation Step -Propagation Steps -Termination Step(s)

B. Monomer Concentration

Monomer is present throughout the reaction, even at the end

C. Polymer Molecular Weight



Step Growth

Distinct and Different Initiation, Propagation and termination are all the same step "Termination" is the last reaction that takes place -Early in the reaction the monomer is depleted -Many dimers and trimers are produced early in the reaction. The monomer is consumed at early stages of the reaction



Reaction must be driven to 99.9% complete to get a polymer

Chain Growth of Poly dimethyl siloxane (PDMS, Silicone)



Sol-Gel Crosslinking





Free Radical Chain Growth

Two Free Radical Initiators



Both are dissociated by heat AIBN is soluble in organic solvents BP in water or organic solvents (BP is explosive)



н c=c-c**:**

Ziegler-Natta Catalysts (Heterogeneous Catalysts)





Polymers have a Dispersion in All Properties

Molecular Weight (Molar Mass)

Stereochemistry

Block Copolymer Composition

Branch Structure



Polymers have a Dispersion in All Properties

Molecular Weight (Molar Mass)

Stereochemistry

Block Copolymer Composition

Branch Structure









Molecular Weight Distribution



$$\overline{M}_{n} = \Sigma x_{i} M_{i}$$

$$DP = \frac{M_{n}}{m}$$

$$\overline{M}_{w} = \Sigma w_{i} M_{i}$$

$$PDI = M_{w} / M_{n}$$

$$M_{w} = \sum_{i} x_{i}^{2} M_{i}$$

$$M_{z} = \sum_{i} x_{i}^{3} M_{i}$$

 \overline{M}

This can be directly related to the Gaussian Distribution

$$n_p = \frac{\int_{n=0}^{\infty} n^p P(n) dn}{\int_{n=0}^{\infty} P(n) dn}$$

$$n_{1} = \frac{\int_{n=0}^{\infty} nP(n)dn}{\int_{n=0}^{\infty} P(n)dn}$$

$$n_{w} = \frac{\int_{n=0}^{\infty} n^{2} P(n) dn}{\int_{n=0}^{\infty} n P(n) dn} = \frac{n_{2}}{n_{1}}$$

Molecular Weight Distribution



$$n_z = \frac{\int_{\infty}^{n^3} P(n) dn}{\int_{n=0}^{\infty} n^2 P(n) dn} = \frac{n_3}{n_2}$$

z-average

$$n_{v} = \left(\frac{\int_{n=0}^{\infty} n^{1+a} P(n) dn}{\int_{n=0}^{\infty} n P(n) dn} \right)^{\frac{1}{a}}$$

 $0.5 \le a \le 0.8$

Viscosity Average



Butadiene has two carbon-carbon double bonds, in the 1 and 3 positions, that is, starting at the carbon atoms numbered 1 and 3.



Note: Cis is Latin, and means "on this side". Trans is also Latin and means "on the other side". You may have seen them in place names like Gallia Cisalpina, meaning "land of the Celts on this side of the Alps", or Transylvania, meaning "land on the other side of the forest".

The top repeat unit is called "*cis*-1,4" because the carbon atoms of the carbon-carbon double bond are both bonded to the backbone chain on the *same side* of the double bond, and because the monomer is linked into the chain through carbon atoms 1 and 4.

The second repeat unit is called "*trans-1,4*" because the carbon atoms of the carbon-carbon double bond, are bonded to the backbone chain on *opposite* sides of the double bond, and again the monomer is linked into the chain through carbon atoms 1 and 4.

The bottom repeat unit is called "1,2" because the monomer is linked into the chain through carbon atoms 1 and 2. It is called "side vinyl" because the vinyl group, that is the carbon-carbon double bond is hanging off chain as a side group, rather than as part of the backbone chain.





Atactic Polmer

Has no tacticity

For a random distribution of tacticity: 50% r and 50% m or 25% isotactic, 25% syndiotactic, 50% heterotactic

Higher order groupings are important to crystallinity, Pentads, Heptads, etc. But there are limits to our ability to resolve tacticity using NMR

Polymer Processing





Figure 15.25 Schematic diagram of an extruder. (Reprinted with permission from *Encyclopædia Britannica*, © 1997 by Encyclopædia Britannica, Inc.)



Figure 15.26 Schematic diagram of an apparatus that is used to form thin polymer films. (Reprinted with permission from *Encyclopædia Britannica*, © 1997 by Encyclopædia Britannica, Inc.)

Figure 15.24 Schematic diagram of an injection molding apparatus. (Adapted from F. W. Billmeyer, Jr., *Textbook of Polymer Science*, 2nd edition. Copyright © 1971 by John Wiley & Sons, New York. Reprinted by permission of John Wiley & Sons, Inc.)

