

(1a)

$$\frac{T_m - T_m^b}{T_m^b} = \frac{2(\gamma_{LW} - \gamma_{SW})}{H \rho \Delta h} \quad \text{--- (1)}$$

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where T_m^b = bulk melting temp.

γ_{LW} & γ_{SW} = liquid-wall / solid-wall surface tension

$$\rho = \frac{N}{V} = \text{density}$$

$$\Delta h = h_L - h_S \Rightarrow \text{latent heat of melting}$$

Gibbs-Thomson eqn

$$T_m(H) = T_m^b + \frac{2(\gamma_{LW} - \gamma_{SW})}{\rho_s A_m H} \quad \text{--- (2)}$$

In the $\mu A_w H T$ ensemble, the thermodynamic potential is the grand potential

$$\mathcal{L} = U - TS - \mu N = -PA_w H + 2\gamma A_w \quad \text{--- (3)}$$

with internal energy

$$U = TS - PA_w H + 2\gamma A_w + \mu N$$

where S = entropy

P = pressure

γ = surface tension

@ coexistence between the liquid & solid phases;

$$\mathcal{L}_L = \mathcal{L}_S$$

$$\text{but } P_L - P_S = \frac{2(\gamma_{LW} - \gamma_{SW})}{H} \quad \text{--- (4)}$$

This depends on the difference in surface tension between the liquid & the walls between the solid & walls, respectively as well as on the pore size (H)

$$d\mu = -s_L dT - p_A w dH + (2\gamma - p_H) dA_w - N d\mu \quad \text{--- (5)}$$

$$(s_L - s_r) dT + \frac{2A_w (\gamma_{LW} - \gamma_{SW})}{H} dH + (N_L - N_r) d\mu = 0 \quad \text{--- (6)}$$

Integrating eqn (6) ultimately [$H \rightarrow \infty$]

$$\frac{dH}{H^2} = - \frac{dT}{2(\gamma_{LW} - \gamma_{SW})} \left[(p_L s_L - p_r s_r) + (p_L - p_r) \frac{d\mu}{dT} \right] \quad \text{--- (7)}$$

where $\rho = \frac{N}{V}$ = density

entropy / particle, $s = \frac{S}{N}$

$$\text{Also; } \frac{d\mu}{dT} = \frac{p_L^b s_L^b - p_r^b s_r^b}{p_L^b - p_r^b} = -s_L^b \quad \text{--- (8)}$$

where b (superscript) = bulk (unconfined) liquid & gas phases.

In the case of isobaric-isothermal liquid phase, the result would be exactly $-s_L^b$

$$\therefore \frac{dH}{H^2} = - \frac{(p_L - p_r)(s_L - s_L^b) + p_r(s_L - s_r)}{2(\gamma_{LW} - \gamma_{SW})} dT \quad \text{--- (9)}$$

For sufficiently large confining distances (corresponding small shift in the melting temp, $T_m - T_m^b$)

Assumption: $|P_L - P_s| \ll P_s$

$$\frac{dH}{H^2} = - \frac{P_s^b \Delta_m s^b}{2(\gamma_{LW} - \gamma_{SW})} dT \quad \text{--- (10)}$$

with $\Delta_m s^b = S_L^b - S_s^b$ being the bulk entropy of melting temp.

Integrating eqn (10) along a thermodynamic path connecting the confined system for finite h & corresponding T_m and an ~~unconfined~~ unconfined one [$h \rightarrow \infty$ and bulk melting temp

T_m^b)

Assumption: ratio on RHS is independent of temp. & confining distance over the considered range.

Under these conditions;

$$\int_H^{+\infty} \frac{dH}{H^2} = - \frac{P_s^b \Delta_m s^b}{2(\gamma_{LW} - \gamma_{SW})} \int_{T_m}^{T_m^b} dT$$

$$\therefore T_m(h) = T_m^b + \frac{2(\gamma_{LW} - \gamma_{SW})}{h P_s^b \Delta_m s^b}$$

(16) Using a "confined Chapeyron" approach in the $UA_{wt}HT$ ensemble: -15

The slit pore has a surface area A_w , a width H & a pore volume $V = A_w H$ [from the fig in the paper]

Assumption: both confining walls are made of the same material so that their interaction with the confined fluid or solid are identical

$$\Omega = U - TS - \mu N = -PA_{wt} + 2\gamma A_w$$

with internal energy

$$U = TS - PA_{wt} + 2\gamma A_w + \mu N$$

where S = entropy

P = pressure

γ = surface tension

@ coexistence between the liquid & solid phases, thermodynamic potentials of the 2 phases are equal $\Omega_L = \Omega_S$

①c) Ostwald - Freundlich Eqn

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$$\Rightarrow x_a = x_a^\infty \exp \left[\frac{2V_a \gamma}{R_a T R_{seq}} \right]$$

where x_a = mole fraction

V = molar volume

R_{seq} = radius

γ = interfacial tension

R_a = gas constant

T = temp

Kelvin eqn $\Rightarrow \ln \left(\frac{p(r)}{p} \right) = \frac{2\gamma V_{molecule}}{k_B T r}$ OFE

$$\frac{\Delta p}{\Delta T} = \frac{p_L}{T^2 R}$$

$$p(r_1, r_2) = p - \frac{\gamma p_{vapor}}{(p_{liquid} - p_{vapor})} \left(\frac{1}{r_1} + \frac{1}{r_2} \right)$$

If particle is assumed to be spherical, then $r = r_1 = r_2$

$$\therefore p(r) = p - \frac{2\gamma p_{vapor}}{(p_{liquid} - p_{vapor})}$$

Since $f_{\text{liquid}} \gg f_{\text{vapor}}$, then $f_{\text{liquid}} - f_{\text{vapor}} \approx f_{\text{liquid}}$

$$\therefore p(r) \approx P + \frac{2\gamma f_{\text{vapor}}}{f_{\text{liquid}} \cdot r}$$

Assuming vapor obeys the ideal gas law:

$$f_{\text{vapor}} = \frac{N_{\text{vapor}}}{V} = \frac{MW \cdot n}{V} = \frac{MW \cdot P}{RT} = \frac{MW \cdot P}{N_A k_B T}$$

Since $\frac{MW}{N_A}$ = mass of one molecule of vapor/liquid

$$\therefore \frac{\frac{MW}{N_A}}{f_{\text{liquid}}} = \text{volume of one molecule} = V_{\text{molecule}}$$

$$\therefore p(r) \approx P + \frac{2\gamma V_{\text{molecule}} P}{k_B T r} = P + \frac{R_{\text{critical}} P}{r} \quad \text{where } R_{\text{critical}} = \frac{2\gamma V_{\text{molecule}}}{k_B T}$$

$$\text{Thus; } \frac{p(r) - P}{P} \approx \frac{R_{\text{critical}}}{r}$$

$$\text{Since; } \frac{p(r)}{P} = 1 - \frac{P - p(r)}{P}$$

$$\text{then, } \log\left(\frac{p(r)}{P}\right) = \log\left(1 - \frac{P - p(r)}{P}\right)$$

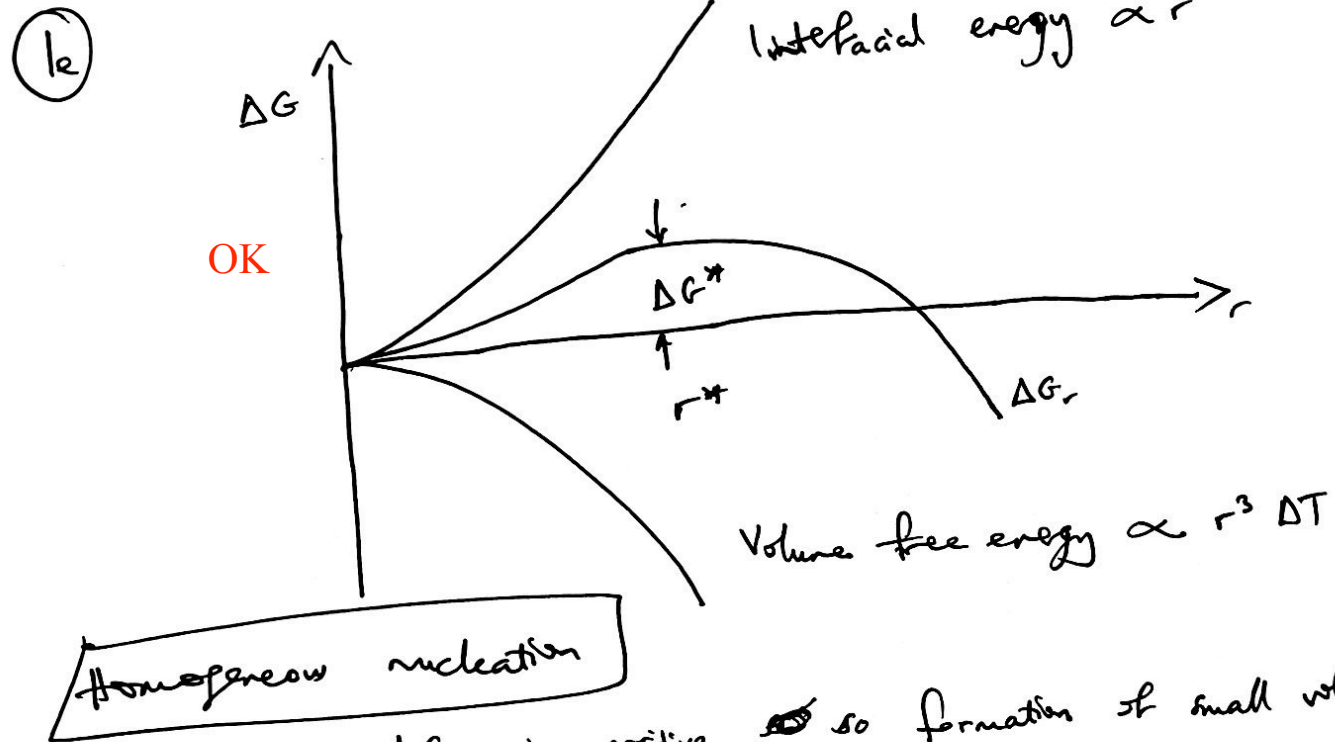
$$\text{since } p(r) \approx P, \text{ then } \frac{P - p(r)}{P} \ll 1$$

$$\text{If } x \ll 1, \text{ then } \log(1-x) \approx -x$$

Hence; $\log\left(\frac{p(r)}{p}\right) \approx \frac{p(r) - p}{p}$

$\therefore \log\left(\frac{p(r)}{p}\right) \approx \frac{R_{\text{entical}}}{r}$

d) -20



Below T_m , ΔG_v is positive, so formation of small volume of solid has negative contribution

If γ_{sl} is isotropic, the shape should be sphere with radius

$$\Rightarrow \Delta G_r = -\frac{4}{3}\pi r^3 \Delta G_v + 4\pi r^2 \gamma_{sl}$$

$$r^* = \frac{2\gamma_{sl}}{\Delta G_v} = \left(\frac{2\gamma_{sl} T_m}{L_v} \right) \frac{1}{\Delta T}$$

Heterogeneous nucleation

$$\Delta G_{\text{heterogeneous}} = \Delta G_{\text{homogeneous}} \times f(\theta)$$

$$\text{where } f(\theta) = \frac{2 - 3\cos\theta + \cos^3\theta}{4}$$

$$r^* = - \frac{2\gamma_{\text{sl}}}{\Delta G_v}$$

②a Type of system: fully isomorphous OK

Determination of composition & amounts of phases

⇒ Lever rule [Using a tie-line]

One would expect that as temperature is reduced and the spherical domains start to form.

$\alpha \Rightarrow 85 \text{ at\% Ni}$

$L \Rightarrow 75 \text{ at\% Ni}$

②b Phase region: Eutectic

OK Triple point: Eutectic

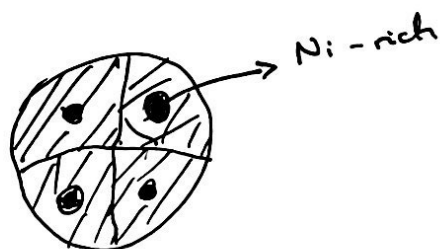
Reaction: $L \rightarrow \text{Ni} + \text{ZrNi}_5$

Gibbs' Phase Rule:

$$F = C - P + 1 \quad [\text{at constant pressure}]$$

$$F = 2 - 3 + 1$$

$$F = 0$$

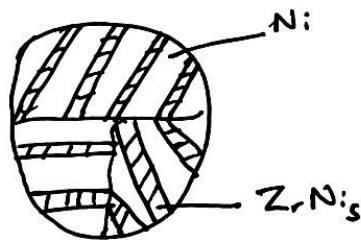


(2d) An intermetallic phase is a chemical compound consisting of 2 or more metals -15

- @ Room temp (R.T) $\rightarrow [1170^\circ\text{C}]$; $\text{ZrNi}_5 = 15 \text{ at\% Zr}$
 @ " " " $\rightarrow [1438^\circ\text{C}]$; $\text{ZrNi}_7 = 22 \text{ at\% Zr}$
 @ " " " $\rightarrow [920^\circ\text{C}]$; $\text{ZrNi}_8 = 25 \text{ at\% Zr}$
 @ " " " $\rightarrow [1163^\circ\text{C}]$; $\text{Zr}_7\text{Ni}_{10} = 41 \text{ at\% Zr}$
 @ " " " $\rightarrow [1180^\circ\text{C}]$; $\text{Zr}_8\text{Ni}_{11} = 28 \text{ at\% Zr}$
 @ $975^\circ\text{C} \rightarrow [1157^\circ\text{C}]$; $\text{Zr}_9\text{Ni}_{11} = 45 \text{ at\% Zr}$

(2c)

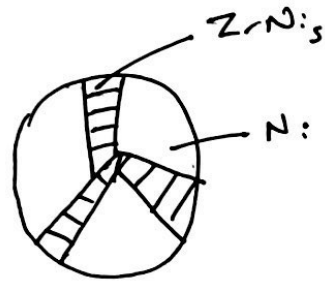
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Quench to the bottom

Phase Fraction of Ni = 0.67
 Zr = 0.33

Composition of Ni = 100% Ni
 = ZrNi5 = 85% Ni



Slow cool

$$\text{Phase fraction of Ni} = \frac{15 - 5}{15 - 0} = 0.67$$

$$Z_r = 1 - 0.67 = 0.33$$

Composition of Ni = 100% Ni

Composition of $ZrN_{1.5}$ = 85% Ni

2e